1	Biodiesel from microalgae in lagoons: an acceptable
2	alternative fuel to the transportation crunch?
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1 ABSTRACT

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One of the major reasons for microalgae popularity as an acceptable fuel source is their

4 potential to maximize the productivity, e.g. gallons of oil or fuel produced per acre per year,

5 converting the energy of solar photons during the process of CO_2 fixation into biomass energy

6 benefiting the environment. Marketing the generated co-products, termed post extraction algal

7 residue (PEAR) could make the transportation fuel viable from microalgae. These self-

8 contained microbial factories can convert sunlight and CO₂ into biofuel are the fastest

- 9 growing plants and 50% of their weight is oil.
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11 The main objective of this research is the qualitative and quantitative analysis of the biofuel

12 obtained from microalgae and focuses on the energetic and environmental feasibility of this

13 fuel for use in the transportation sector. This evaluation includes the identification of the

14 obstacles and limitations of the process in terms of energy and environmental performance.

15 Another important aspect of this work is the need for improvement of product processing and

16 recovery that includes mechanical and energy intensive processes like centrifugation,

- 17 filtration, flocculation, and cell disruption.
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19 The results obtained so far show that the various strains of microalgae used (nearby lagoons in

- 20 Portugal and Spain) offer a huge prospect of biodiesel production.
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- 22 KEYWORDS: Biodiesel, microalgae, alternative fuel, lagoon.
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1. MOTIVATION 1

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The current oil crisis and the fast depletion of conventional fossil oil reserves have made it 3 more imperative for organizations and countries to invest more time and efforts in research on 4 suitable renewable feedstock. It is known that algae grown in CO_2 enriched environment can 5 be converted to oily substances and hence can contribute to the solution of two major 6 problems: 7

a) Reduction of gaseous emissions (fossil CO₂, nitrogen and sulphur oxides), namely 8 greenhouse gases (GHGs). 9

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b) Shortage of energy sources without compromising food production capacity.

The increasing fuel demand worldwide, rapid rise of crude oil price, limited reserves 11 and the effects of fossil fuel use on the environment has pushed scientists to look for cleaner, 12 renewable fuels. Biodiesel fuel has received considerable attention with its biodegradable, 13 renewable and non-toxic characteristics. However, the production of biodiesel from cultures 14 such as sun flower or rapeseed has several problems, namely: competition with food cultures, 15 risk of distortion of food prices, effective reductions in terms of GHGs emissions, and need of 16 environmental sustainability criteria for biofuels production. The main rationale underlying 17 biodiesel utilisation emerges from the need to find an alternative energy source for the 18 19 transportation sector.

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2. THE ENERBIOALGAE PROJECT 22

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The EnerBioAlgae Project is being developed during 2011-2012 as a part of the SUDOE 24 Program (Territorial Cooperation Operational Program of Southwest Europe 2007-2013). The 25 main goal is to study the potential for biodiesel production from microalgal species and its 26 overall Life Cycle Analysis (LCA). The project partnership consists of three entities in Spain 27 (University of Vigo as Coordinator, University of Almería and Inega - Energy Institute of 28 Galicia), two in France (University of Pau and Pays de l'Adour and the Centre National de la 29 30 Recherche Scientifique) and one in Portugal (University of Aveiro). 31

The secondary objectives of the project are:

- To refine the system of production of algal biomass for energy purposes in order to 32 33 improve yields;
- To develop the methodological aspects and enhance the technical, economical, 34 environmental and energetic potential of microalgae; 35
- To identify, locate and use the degraded water resources for high potential energy 36 sources in Galicia (Spain), Almería (Spain) and Aveiro (Portugal); 37
- To develop instrumentation technologies for online monitoring and control of algae 38 cultures with a system based on the use of LIDAR technology and pattern recognition 39 algorithms that reveal the state of the algae at real time; 40
- To optimize the quality of biodiesel produced from microalgae (fulfilling the 41 European regulation) to encourage public and private investment; 42
- To execute a complete economic analysis of the microalgae-derived biodiesel 43 44 production;
- To evaluate and demonstrate the technical, economical and energy feasibility of the 45 developed environmental technologies and to develop an overall well to wheel 46 47 (WTW) LCA for the evaluation of the environmental impacts of the production of biodiesel from microalgae. 48
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1 This research can be divided into five main tasks: a) allocation of resources, 2 identification and characterization of the strain; b) selection and growth of suitable microalgae 3 under proper conditions; c) online monitoring of the algae; d) extraction procedures; and e) 4 analysis and characterization of the obtained oil.

The project integrates the protection and conservation of the environment, combating 5 climate change, diversification of energy supplies, development and exploration of alternative 6 energy and biodiversity. The use of microalgae as an energy source for conversion into 7 biofuels has excellent prospects, with potential competitive advantages. The aim is to achieve 8 maximum profitability of the energy production on an industrial scale, which requires more 9 investment in research applied to various fields of technology and supported by pilot 10 experiments for demonstration purposes. The EnerBioAlgae project addresses these needs 11 while contributing to the improvement of the environment by integrating the use of 12 contaminated water and CO₂ capture. Furthermore, microalgae cultivation does not compete 13 with food production, does not require large area or fertile terrains and maximizes water 14 15 savings. Microalgae cultivation offers significant environmental benefits when compared with crops such as rape, sunflower, jatropha etc. However, biodiesel from microalgae is still more 16 expensive than conventional diesel. A recent estimate states that the cost of microalgae-17 derived biodiesel is on a 20 fold range over conventional diesel oil (1). 18

The enhancement of the energy potential from a given territory and the mitigation of environmental issues on degraded water resources derived from EnerBioAlgae will stimulate the growth of the renewable energy sector in Southwestern Europe, contributing to energy diversification, reducing the dependence on fossil fuels and ensuring a quality supply of energy under the European standards.

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26 **3. LITERATURE REVIEW**

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Several authors addressed the production of biofuel from microalgae as a promising source addressing the issues of the current oil crisis and the greenhouse and global warming problems.

US DOE launched the National Algal Biofuels Technology Roadmap (2) that lays the groundwork for identifying challenges that will likely need to be surmounted for algae to be used in the production of economically viable, environmentally sound biofuels.

11.6 million tonnes of fuel were consumed in Portugal in 2011 (3). To satisfy that need by resorting to microalgae with an average lipid content of 30% requires only 3200 km² land while if sunflower cultures were used an area of about 4 times the area of Portugal would be required (4).

In order to satisfy demand it is important to choose the most suitable microalgae (in terms of lipid content and growth rate) for biodiesel production, both from the points of view of quantity and quality of the oil. Physical (light and temperature), chemical (nutrients and CO₂) and biological factors (virus infections or contaminations) affect the growth of algae. The factors can be handled externally in order to produce high oil content biomass for biodiesel. Figure 1 lists the oil content of various microalgae and the factors influencing the growth rate of the microalgae.

	-				20. 20.
	Factors that influenc	e algal grow th in	a high	rate algal pond	33
	Abiotic factors	Light (quality	r, quanti	ty)	
	Physical and chemical	Temparature			
		Nutrient Cor	ncentrati	on	
		O_2, CO_2			
		pH			
		Salinity	-		
1	Disting and	I oxic chemi	loxic chemicals		
	BIOLC FACTORS	Pathogen (ba	icteria, r	ung, viruses) Ictor	
		Competition	Freuation of zooplankton		
	Operational factors	Mixing	Derw cerr	species	
	opududidi dovato	Dilution rate			
		Depth			
		Addition of b	icarbon	ate	
		Harvestingfr	equency		A)
<u>Microalga</u>	<u>0</u>	il Content (% dry	wt)		
Botrvococcus br <i>a</i> unii		25-75			
Chlorella sp.		28-32			
Crypthecodinium cohnii		20			
Cylindrothec a sp.		16-37			
Dunaliella primolecta		23			
Isochrysis sp.		25-33			
Monallanthus salina		> 20			
Nannochloris sp.		20-35			
Nannochloropsis sp.		31-68			
Neochloris oleoabundans		35-54			
Nitzschia sp.		45-47			
Phaeodacty lum tricornutu	m	20-30			
Schizochytrium sn		50-77			
Tetraselmis sueica		15-23	B)		

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FIGURE 1 A) oil content of various microalgae strains (5); B) the growth rate of algae influenced by physical, chemical and biological factors (6)

Algae basic needs include water, sunlight and CO₂. Nutrients such as nitrogen (N), 5 phosphorous (P) and potassium (K) can serve as fertilizer for the algae growth. Silica, iron 6 and several trace elements can be considered as important marine nutrients. Potential algae 7 biodiesel manufacturers can build biodiesel plants close to the energy manufacturing plants 8 that produce lots of carbon-dioxide. The basic reaction in water is $(CO_2 + light energy + H_2O_2)$ 9 = glucose + O₂ + H₂O). 10

Some authors developed a study in which sea water was supplemented with commercial 11 nitrate and phosphate fertilizers and a few other micronutrients for growing marine microalgae 12 (5). Sawayama et al. used some of the CO_2 that is released in power plants by burning fossil 13 fuels for the growth of the microalgae (7). Other authors found that beside carbon, nitrogen is 14 the second most important nutrient to microalgae growth since it may comprise more than 10% 15 of the biomass. Nitrogen can be present in many forms, but the most common nitrogen 16 compounds assimilated by microalgae are ammonium (NH_4^+) and nitrate (NO_3^-) (5, 8). 17

The microalgae cultivation is followed by extraction and esterification. Extraction 18 methods are used to convert the chemical energy contained in the grown microalgae into 19 high-value oils with minimal fossil energy consumption if possible. Triglycerides or 20 triacylglycerol's have a glycerin backbone joined by ester linkages to three fatty acid chains. 21 The fatty acid portion varies in length between twelve and eighteen carbons. Biodiesel 22 molecules are mixture of fatty acids methyl esters (FAMEs) produced from a reaction named 23 transesterification. 24

There are several physical (Mechanical crushing, Osmotic shock, Ultrasonic extraction) 1 and chemical (Hexane, Soxhlet, Enzymatic, Supercritical fluids) extraction processes for 2 extracting lipids from dry or wet algal biomass. Some authors mentioned that the combination 3 of sonoenzymatic treatment accelerates extraction and increases the yield (9). Other authors also 4 5 address that the supercritical alternative is suitable for the biodiesel production from a technical point of view; however, from an economic analysis, it does not appear to be good (10-13). 6 Some other procedures were proposed by Bligh and Dyer (14), who used solvent mixtures 7 made of chloroform or methanol and ethanol or diethyl ether. Combining methods like 8 9 microwave heating and Soxhlet extraction, reduced the extraction time from 8 hours to 32 10 minutes (15).

The oil extraction process through the wet route consumes 2.8 times more energy than dry route (*16*). Fossil energy ratio (FER) of the dry route is slightly higher than that of the wet route. High FER of the dry route benefits from the high thermal efficiency (95%) of the pyrolysis process. Figure 2 shows the detailed dry and wet routes from microalgae production to biofuel.



FIGURE 2 Microalgae-to-biofuel route, (a) the dry route; (b) the wet route (16)

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4. METHODOLOGY

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In our work we have investigated the potential of the biodiesel produced from different 3 4 microalgae strains like Chlorella vulgaris, Scenedesmus, Chlorophyta and Nannochloropsis grown in laboratory conditions. Early research on Chlorella vulgaris acknowledges that the lipid content by weight of dry mass under normal development is about 14%, while in 6 freshwater by nutrient deprivation is 40% by weight of dry mass (17).

A Pugh matrix (also known as Criteria Based Matrix) will be developed, in order to 8 create a decision support tool that studies different criteria, for comparison of the trade-offs 9 between them and also will highlight how the phases of the biodiesel from microalgae 10 production can be optimized. Development of a Pugh Matrix plays a crucial role in the 11 present proposal since this methodology will help to determine which potential solutions are 12 better (based on criteria). It will be used for the selection between several viable choices with 13 different options in order to assign scores relative to the criteria. More reliable results will be 14 15 obtained if scores assigned are based on reliable data from the process. The expected results include a technical and economical characterization of the microalgae processing phases and 16 biodiesel production, an economic model of the processing phase and a Life cycle assessment 17 of the biodiesel production from microalgae. The developed LCA will appear as a decision-18 making tool. Since different levels of lipid production of microalgae will be obtained and 19 knowing that biodiesel should specify quality regulations, the economic analysis appear to be 20 the best chain of processes in its broadest sense, i.e. integrating LCA. 21

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4.1. Experimental procedure 24

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A photobioreactor (PBR), consisting of a stainless steel structure, 6 acrylic columns of 110 26 mm outer diameter and 10 fluorescent tube lights TLD 36W/865, each column with an 27 28 approximate volume of 5 L, was used for the microalgae culture. There were two pH and temperature sensors placed in the middle of two columns. An initial inoculum of half liter per 29 30 column of microalgae strain was used. Nutrients were added on an everyday basis.

For the cultivation the pH was maintained between 7.2 - 7.5, the culture temperature 31 was around 22°C and a photo-period of light/dark for 12 hours was used. Everyday 80ml of 32 33 samples were collected from each columns and the same amount was restored by adding water and nutrients in order to calculate the cell growth on a daily basis. The maximum 34 growth of cells was reached on the 9th day of culture. Figure 3 shows the PBR used for the 35 cultivation of algae in our study and the culturing steps. 36



FIGURE 3 Culture in column PBR installed in the University of Aveiro and extraction of samples

6 Several strains were tested in the PBR, namely Chlorella, Chlorophyta and 7 Scenedesmus. In addition, lyophilized biomass of Nannochloropsis and Scenedesmus were 8 sent from Almería region to the University of Aveiro, for oil extraction.

9 Then, algal biomass was gathered, centrifuged and eventually transformed into a 10 paste-like wet substance. Both wet and dry extraction were conducted with the cultured algae biomass. Lyophilized biomass was used for dry extraction process. The extraction process 11 included magnetic stirring, vacuum filtration and ultrasound. The extracted oil after trans-12 esterification was characterized by GC. In our work the wet extraction procedure as a 13 modification of method by Bligh and Dyer (14) was used to extract the lipid in micro algal 14 cells. Extraction and partitioning of the lipids are synchronal in the Bligh and Dyer method 15 (14) following an equilibrium theory. Addition of methanol can be one of the key parameters 16 for the improvement of the lipid content following the extraction kinetics. Hence, tissues 17 homogenized with chloroform-methanol are possibly the best lipid extractant despite the 18 environmental and health hazards are likely to accompany it (19). 19

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21 4.2. Quality analysis

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The crucial point for the production of high quality biodiesel is the fidelity to biodiesel fuel standard specifications, EN 14214 (2003). Within EN 14214, method EN 14103 specifies the Fatty Acid Methyl Ester (FAME) and Linolenic Acid Methyl Ester (LAME) content, which is used to profile the vegetable or animal oil feedstock used in biodiesel production. The FAME analysis was carried out with a split injection into an analytical column with polar stationary phase and an FID detector.

The equipment used here is the Varian 3800 Gas Chromatograph (GC), fitted with a capillary injector and FID. The inlet temperature was 220° C, the injection volume was 2μ L, the oven final temperature was 200° C and the column configuration is DB1-ht, 15 m, (0.32 mm x 0.1 μ l).

An analysis based on the FAME, composition of saturated and unsaturated methyl esters, LAME and iodine value predicts the critical parameters and the overall potential of the biodiesel. It was concluded that the quality of biodiesel strongly depends on the growing process that should be optimized for the mass production. The technologies employed to FAME is determined by:

purify and transform the feedstock into fatty acid alkyl esters determined whether the oil produced meets the specification standards but also conditions of the produced quantity of free and bonded glycerin which in return defines the purity and quality of the biodiesel.

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$$=\frac{\sum A - A_{IS}}{A_{IS}} \times \frac{C_{IS} \times V_{IS}}{m} \times 100\%$$

Where:

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9	$\sum A = \text{Total peak area } C_{14:0} - C_{24:1};$
10	A_{IS} = internal standard (methyl heptadecanoate) peak area;
11	C_{IS} = concentration of the internal standard solution, in mg/mL;
12	V_{IS} = volume of the internal standard solution used, in mL;
13	m = mass of the sample, in mg.
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According to EN14103, the result for the total FAME content should be higher than 90% (20). Also, the method of oil extraction can directly influence the fatty acid profile of the lipid content of microalgae depending on the efficiency of extraction of polar and neutral lipids (21).

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LAME is calculated by:

$$L = \frac{A_L}{\sum A - A_{IS}} \times 100\%$$

21 Where:

22 $\sum A = \text{total peak area } C_{14:0} - C_{24:1};$

23 A_{IS} = internal standard (methyl heptadecanoate) peak area;

- 24 A_L = linolenic acid methyl ester peak area.
- Total linolenic acid ($C_{18:3}$) content should be higher than 1 % and lower than 15 % (21, 22).

The mass of iodine in grams absorbed by 100 grams of a chemical substance isby definition a measure of total unsaturation compounds in the fatty acids. The EN14214 specification allows a maximum of 120 for the iodine number (*23*).

Indine value =
$$X g$$
 indine / 100 g sample Eq. 3

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- 34 **4.3. Life Cycle Assessment**
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A LCA broadens the scope from environmental impacts to three dimensions of sustainability (people, planet and prosperity) (24). For this task the GREET model (developed by the Argonne National Laboratory) (25) was updated and adapted (since it contemplates the U.S. reality) in order to carry out the LCA of biodiesel from microalgae for the Portuguese reality. For the WTW analysis, a case study based on the 300kms route between Lisbon and Porto, using a passenger vehicle, was considered.

Eq. 1

Eq. 2

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5. RESULTS AND DISCUSSION

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4 5.1. Chlorella vulgaris from Aveiro region, Portugal

5 Figure 4 shows the fatty acid methyl ester (FAME) profile of wet extraction of biodiesel from

6 Chlorella vulgaris while Table 1 shows the LAME and iodine value in accordance to the

- 7 European standard. Total FAME is approximately 95 %.
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FIGURE 4 FAME profile of wet extraction of biodiesel from Chlorella vulgaris

TABLE 1	LAME and	iodine	value of	Chlorella	vulgaris
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Samples	LAME (%)	Iodine Value (%)
Column 1	13	13
Column 2	9.4	9.4

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Results confirm that Chlorella vulgaris grown with the lagoon water of Aveiro region in Portugal with an appropriate methodology and correct execution offers good potential to produce high quality biodiesel in accordance to the European standard.

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20 **5.2.** Chlorophyta and Scenedesmus from Aveiro region, Portugal

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Chlorophyta and Scenedesmus were cultured in parallel in the PBR using the water collected nearby the lagoon of Aveiro, in Portugal. Half of the biomass samples were kept for lyophilization (freeze-drying) in order to perform the dry extraction process. The remaining half was used for the wet extraction procedure.

Figure 5 shows FAME profiles with comparison between the wet and the dry extraction process, respectively for Chlorophyta and Scenedesmus. FAME analysis with wet extraction steps confirms that both the algae types are having high and almost equal potential in the production of biodiesel.



FIGURE 5 FAME - A) Chlorophyta, B) Scenedesmus: Comparison of extraction processes, C) potential of the microalgae strains

Thus FAME analysis confirms that the dry extraction techniques are more effective in 7 order to produce high quality biodiesel irrespective of the microalgae type. Also, both the 8 algae strains have equally high potential to produce quality biodiesel for the transportation 9 10 sector.

LAME and Iodine values confirm both the strains to be have an high potential according to the EU standard, as presented in Table 2. 12

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TABLE 2 LAME and iodine values from Chlorophyta and Scenedesmus

Samples	LAME (%)		Iodine	Value (%)
	Wet (%)	Dry (%)	Wet (%)	Dry (%)
Chlorophyta	5.59	5.3	48.445	48.827
Scenedesmus	2.38	2.015	34.14	51.58

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18 An integrated triangular graph (Figure 6) was plotted representing all the compounds (saturated, monounsaturated and polyunsaturated) in order to compare different parameters in 19 20 respect to the European Standard EN 14214. The explanation of the colors is as follows: yellow (right), good cetane number and iodine value; yellow (left), good Cold filter plugging 21 point (CFPP); green (intersection), biodiesel that satisfies UNE-EN 14214; orange, interest in 22 biodiesel production is zero. The results obtained are in the area that meets the limit of the 23 24 Cetane number and Iodine value (yellow area, right), which show a high content of saturated methyl esters according to the European standard EN14214. The most principal versed topic 25 related to the iodine value of biodiesel is the oxidation stability since the oxidation process 26 affects the fuel quality (23). Thus, both microalgae Chlorophyta and Scenedesmus offer high 27

- 1 potential for biodiesel production with an appropriate methodology and proper execution. Dry
- 2 extraction process produces better results compared to the wet extraction process.
- 3 4



Saturated FIGURE 6 Distribution of monounsaturated, polyunsaturated and saturated methyl esters – Chlorophyta and Scenedesmus (Aveiro, Portugal) 5.3. Nannochloropsis and Scenedesmus from Almería region, Spain Table 3 shows the total FAME and LAME values of the microalgae grown with local resources of Almería, Spain.

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TABLE 3 Potential strain in accordance to the EU standard

Samples	Total FAME %	Total LAME %
1. Nannochloropsis [N]	99.56	10.23
2. Scenedesmus [S(1)]	100	4.5
3. Scenedesmus [S(2)]	99.96	7.46

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Figure 7 shows the good biodiesel production capability potential of all the strains. All the strains are in the green region of the graph, which means a very high and striking potential of the biodiesel production, both in terms of quality and quantity.



FIGURE 7 Distribution of monounsaturated, polyunsaturated and saturated methyl esters – Nannochloropsis and Scenedesmus (Almería, Spain)

5.4. Life Cycle Assessment

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The preliminary results from LCA using the GREET model (updating it with data from the 9 Portuguese reality, such as the electricity production mix, types of trucks and their European 10 emissions regulations, types of trains, distances from the sea transportation sector) lead to the 11 12 conclusion that biodiesel from microalgae is presented as a valid option to replace conventional fuels. For a WTP analysis, the reduction of GHGs emissions can go from 176% 13 14 to 629% when compared with diesel. These values are obtained taking into account that the CO2 source is located in the same place of the biodiesel production. The transport of CO2 by 15 16 heavy duty truck, when necessary, makes the biodiesel production process energetically and environmentally unviable, since energy consumption and GHGs emissions are at least 100% 17 higher when compared to conventional fuels. 18

In a WTW analysis, the use of BD30 (30% of biodiesel mixed with 70% of diesel) 19 presents a 42% lower fuel consumption than diesel; with BD50 and BD100, for BD50 and 20 BD100 mixture the consumption increases between 20% and 40% respectively, relatively to 21 BD30. When there is the need of transporting CO2, the energy consumption values are 22 23 between 165% and 425% higher than a diesel vehicle. Regarding GHGs emissions, values are 82% lower than diesel for the BD100, presenting the emission of 33g of GHGs per km. In the 24 25 stages of raw material and biofuel production there is a capture of 119 grams of GHGs from the atmosphere, making these stages environmentally positive. 26

27 It must be emphasized that while growing microalgae CO2 is used in diluted form. 28 Even under the laboratorial conditions used in the PBR, CO2 was diluted in air. Also, pilot installations for microalgae cultivation do not attempt to separate CO2 from other combustion 29 products. During LCA no attempt was made to address the issue of CO2 extraction and 30 separation. The effects have not been considered because the main focus of our study was to 31 produce high quality and quantity biodiesel from local algae strains and no attempts were 32 considered concerning CO2 extraction and separation from other combustion gases. A LCA 33 of the overall WTW is under development. 34

1 6. CONCLUSIONS AND FUTURE RESEARCH DIRECTIONS

This research has attempted to select microalgae from lagoons in order to produce an environmentally sound alternative fuel. CO₂ emissions have become a huge threat which can be solved by producing a fuel which uses CO₂ during its production. Microalgae can be a solution to solve this problem without compromising land resources for their production. Microalgae can be grown with degraded or wastewater and with CO₂ Intake. Choosing an inexpensive extraction process and reusing the co-products will help the feasibility of mass production of biodiesel.

Based on the values of the percentages of fatty acid methyl ester, saturated and 9 unsaturated acids, linolenic acid methyl ester content and iodine factor, this research shows 10 that the various strains of microalgae used offer a good prospect for biodiesel production. The 11 production of the oil from dry algae biomass (dry extraction steps) gives better results than 12 that obtained from the wet method, which contradicts some of previous work. The work was 13 performed with the local strains of algae and algae biofuel extraction depends a lot on the 14 particular strain and on the region of culture. The particular focus of the project was to come 15 16 up with the potential biodiesel from local microalgae, both in terms of quality and quantity.

Further research will focus on the optimization of the algae growth conditions and the extraction steps (mechanisms leading to increased efficiency) enhancing the mass production of the biodiesel. Also, research with more varieties of microalgae strains is important in order to find the most viable and the best potential biodiesel source. Finally, LCA will be improved. It must be emphasized that the work conducted so far and described in this article does not assure commercialization at this stage, namely because the extraction and transterification procedures, although adequate from a laboratorial point of view, lack scalability.

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